PATENT SPECIFICATION

NO DRAWINGS

1.073,856

No. 32044/65.



Inventor: NORMAN CURTIS COOKE

Date of filing Complete Specification: June 10, 1966.

Application Date: July 27, 1965.

Complete Specification Published: June 28, 1967.

© Crown Copyright 1967.

Index at acceptance:—C2 C(3A10A4C, 3A10A5A1)

Int. Cl.:—C 07 c 51/52

COMPLETE SPECIFICATION

Production of Sodium Acrylate

We, THE DISTILLERS COMPANY LIMITED, of 12 Torphichen Street, Edinburgh 3, Scotland, a British Company, do hereby declare the invention, for which we pray that a patent may be granted to us, and the method by which it is to be performed, to be particularly described in and by the following state-

This invention relates to a process for the

production of sodium acrylate.

It has been proposed to produce sodium acrylate by mixing together aqueous solutions of sodium hydroxide and acrylic acid in approximately stoichiometric amounts. Because of the relatively high solubility of sodium acrylate in water, the resultant aqueous solution must be evaporated to recover solid sodium acrylate. It is necessary to evaporate under reduced pressure because of the tendency of sodium acrylate to polymerise at elevated temperature. Even under the most favourable conditions the sodium acrylate produced contained considerable amounts of polymer. Furthermore, evaporation of water from the aqueous solution is costly in terms of energy requirements.

It is an object of the present invention to produce sodium acrylate by a route in which the disadvantages mentioned above are miti-

gated or obviated.

According to the present invention there is provided a process for the production of sodium acrylate in which a solution of sodium hydroxide in methanol and a solution of acrylic acid in methanol are mixed together, whereby a precipitate of sodium acrylate is produced, and the precipitate is subsequently separated from the methanol solution.

The strength of the solutions of sodium hydroxide and acrylac acid can vary to some considerable extent, but suitable strengths are 25% w/w and 50% w/w respectively. The relative proportions of sodium hydroxide and acrylic acid are preferably stoichiometric. In order to minimise polymerisation, the solution

of sodium hydroxide in methanol is most suit-

ably added to the solution of acrylic acid in methanol within the temperature range 5° to 50°C. The solutions can be mixed batchwise or continuously, for example by means of a

The precipitated sodium acrylate can be separated from its mother liquor, for example by centrifugation or filtration. The mother liquid from which the sodium acrylate is separated can be recycled to become the solvent for a fresh quantity of acrylic acid. If the mother liquor is recycled it should not be used as a solvent for the sodium hydroxide, since strong sodium hydroxide has a deleterious effect on the residue of sodium acrylate present in the mother liquor.

The separated sodium acrylate can be dried, preferably at a temperature below 40°C.

The following examples illustrate the inven- 65

Examples 1-8

A solution of sodium hydroxide of the strength and amount shown in the table was slowly added to a solution of acrylic acid in methanol of the strength and amount shown in the table. The acrylic acid solution was contained in a stainless steel bucket, stirred during the addition of sodium hydroxide, and maintained at a temperature within the range 5-30°C by means of a cold water bath. The resultant precipitate was filtered off and dried in an oven below 40°C.

The mother liquor from which the precipitate was separated in Example I was used to dissolve the acrylic acid in Example 2. The mother liquor from Examples 2-8 was evaporated to yield a further 954 gm of solid which was analysed as 93.6% sodium acrylate and 3.7% sodium polyacrylate.

The dried precipitates from Examples 1 and -8 were intimately mixed. 1 gram of the mixed precipitates gave a clear solution in 10 ml of 50% isopropanol. In a 6 in. Lovibond cell, this solution had colour of 0.6Y, 0.4R and 0.3B.

70

[Price 4s. 6d.]

Prior II

Example	1	2	3	4	5	6	7	8 .
Acrylic acid (gm) Fresh methanol (gm) Recycle mother liquor	1080 1110	1080	1080 1110	1080 1110	1095	1080	1080	2160 1813
methanol (gm) Recovered methanol (gm)		1110			1100	1100	1100	
Sodium hydroxide (gm) Methanol (gm)	600 1920	600 1920	600 1920	600 1920	605 1950	600 1900	600 1900	1200 3840
Time taken to complete addition (hrs.) Temperature	1.0 30 max	2.5 30	3.0 25	3.0 25	0.8 12— 24.5	1.0 30 max	1.1 12— 25	2.7 5.5— 20.5
Dry weight of precipitate (gm)	1140	1205	1135	1162	1137	1168	1137	2297
Analysis of precipitate (% w/w) Sodium acrylate Sodium polyacrylate Water Acidity (acrylic)	98.6 0.7 — trace	99.0 0.2 — neutral	99.1 0.5 — trace	98.3 1.7 — trace	99.2 0.4 — neutral	99.4 0.7 — neutral	98.5 0.3 — trace	99.2 0.2 0.03 neutral

WHAT WE CLAIM IS:—
1. A process for the production of sodium acrylate in which a solution of sodium hydroxide in methanol and a solution of acrylic acid in methanol are mixed together, whereby a precipitate of sodium acrylate is produced, and the precipitate is subsequently separated from the methanol solution.

2. The process according to claim 1 wherein the concentration of the sodium hydroxide solution is 25% w/w.

3. The process according to Claim 1 or 2 wherein the concentration of the acrylic acid solution is 50% w/w.

4. The process according to any of the preceding claims wherein the sodium hydroxide and acrylic acid are reacted in stoichiometric proportions.

5. The process according to any of the preceding claims wherein the solution of sodium hydroxide is added to the solution of acrylic acid at a temperature in the range from 50 to 50°C.

25

6. The process according to any of the pre-

ceding claims wherein the sodium acrylate is separated from the mother liquor by centrifug-

7. The process according to any of the preseparated from the mother liquor by filtration.

8. The process according to any of the preceding claims wherein the mother liquor from which the sodium acrylate is recovered is recycled as solvent for acrylic acid in the re-

9. The process according to any of the preceding claims wherein the sodium acrylate is dried at a temperature below 40°C.

10. A process for the production of sodium acrylate with particular reference to the examples herein.

11. Sodium acrylate whenever produced by the process of any of the preceding claims.

> F. S. M. GRYLLS Agent for the Applicants Great Burgh, Epsom, Surrey.

Leamington Spa: Printed for Her Majesty's Stationery Office, by the Courier Press. -1967. Published by The Patent Office, 25 Southampton Buildings, London, W.C.2, from which copies may be obtained,